



POWERSTEP

YOUR FLUSH, OUR ENERGY

FULL SCALE DEMONSTRATION OF ENERGY
POSITIVE SEWAGE TREATMENT PLANT
CONCEPTS TOWARDS MARKET PENETRATION



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- **17/05/2018, POWERSTEP Conference, Munich**



Funded by
the Horizon 2020
Framework Programme
of the European Union

Grant agreement No. 641661



POWERSTEP

**POWERSTEP technologies lead to
energy-positive WWTPs**
(a market validation by carrying out energy audits)



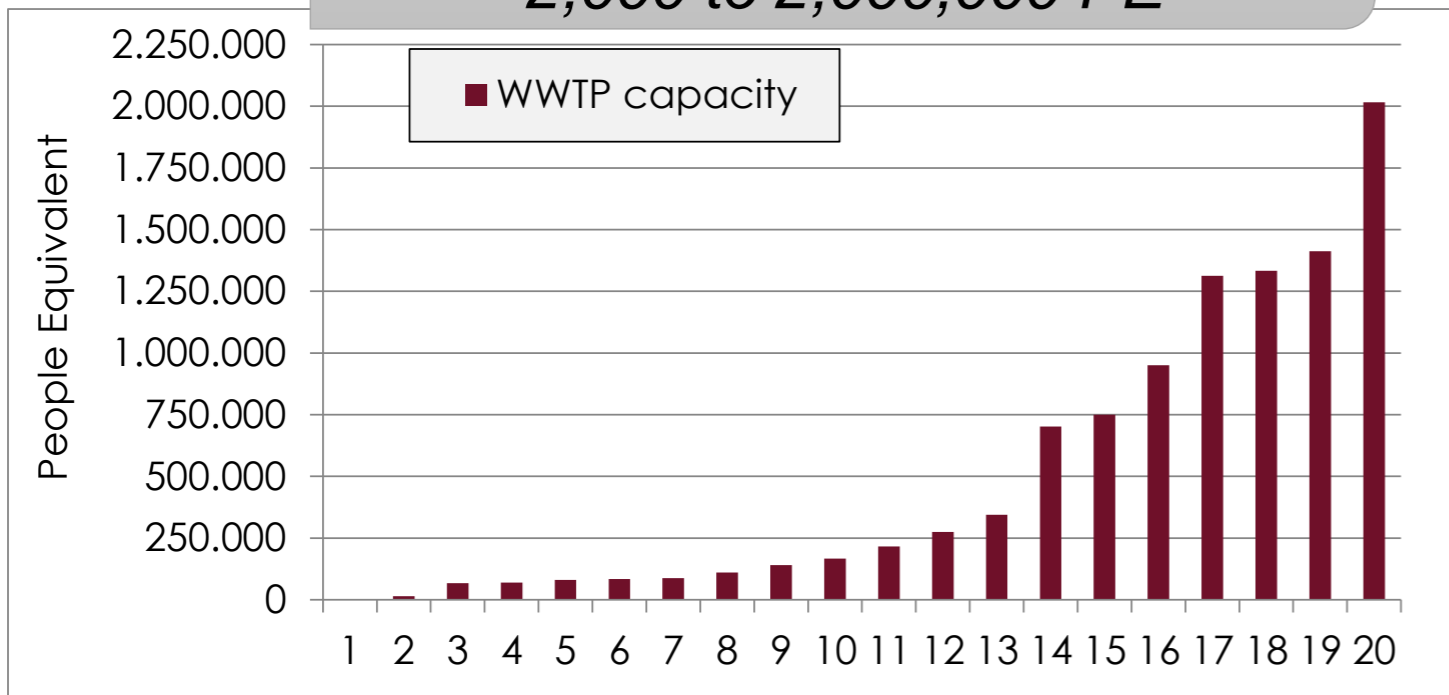


Powerstep evaluation in existing WWTP



20 WWTP out of 38 candidates

from small to big WWTP
2,000 to 2,000,000 PE



in 9 countries



from low to high loading rates
40% to 150% in average

from low to high
discharge requirements
only C removal to TN 8 mg/l

from low to high
electricity consumption
16 to 92 kWh/(PE · a)





Powerstep audit concept



1st step

- Current situation assessment



2nd step

- Optimisation through state-of-the-art measures



3rd step

- Optimisation through Powerstep concepts

Conventional
energy audit



Water2Energy

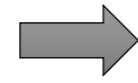
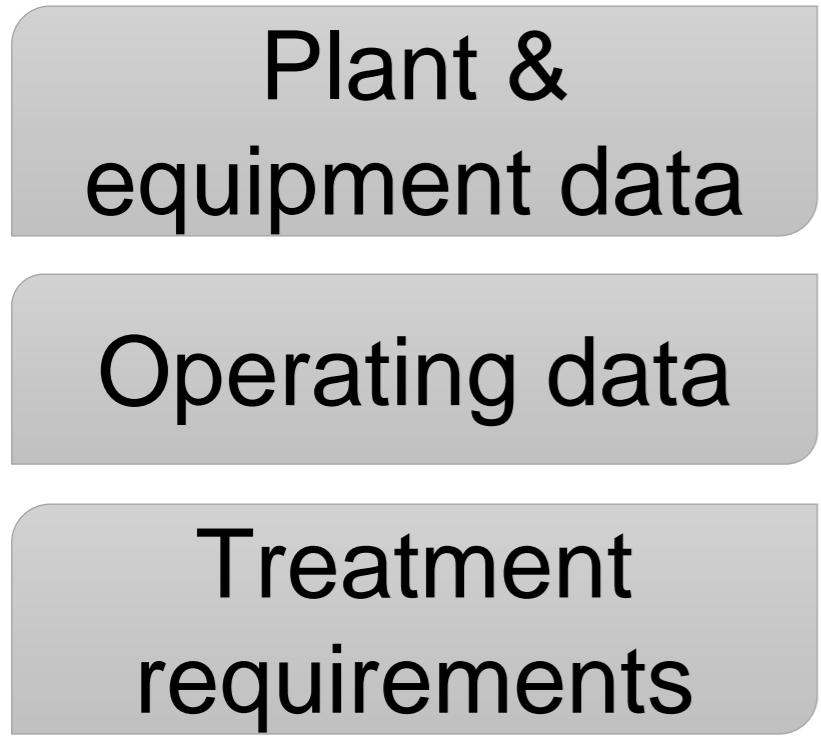
Goal: assess the real potential of Powerstep concepts



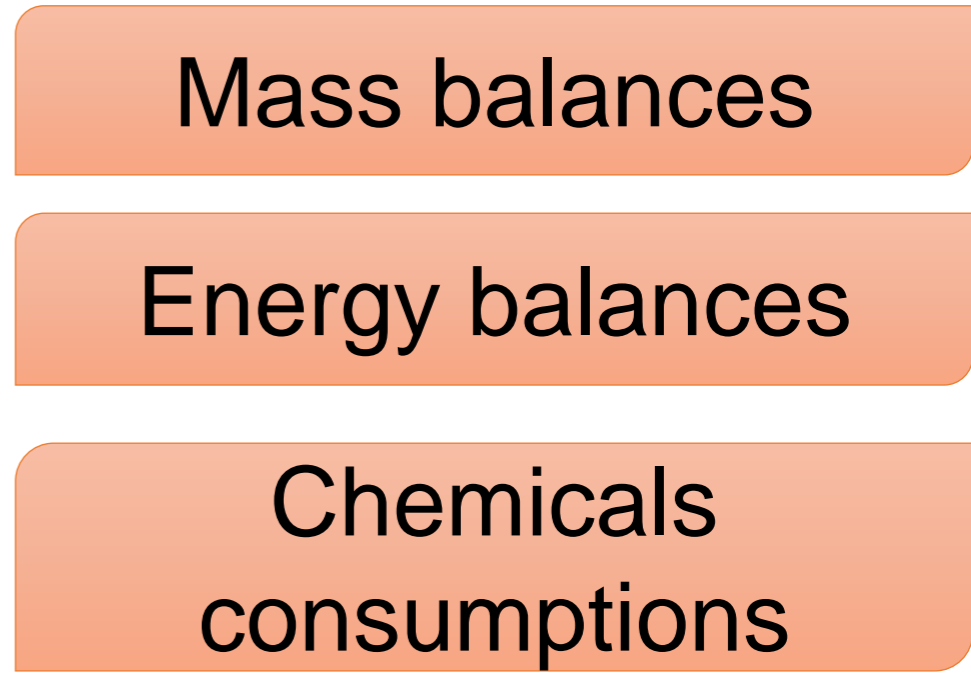
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OCEAN software



proven in more than 100 WWTP worldwide



- ✓ Can be used with low amount or quality of data
- ✓ Data consistency check
- ✓ KPI calculation & comparison with benchmarks
- ✓ Easy calculation of optimisation measures & impact on the whole WWTP

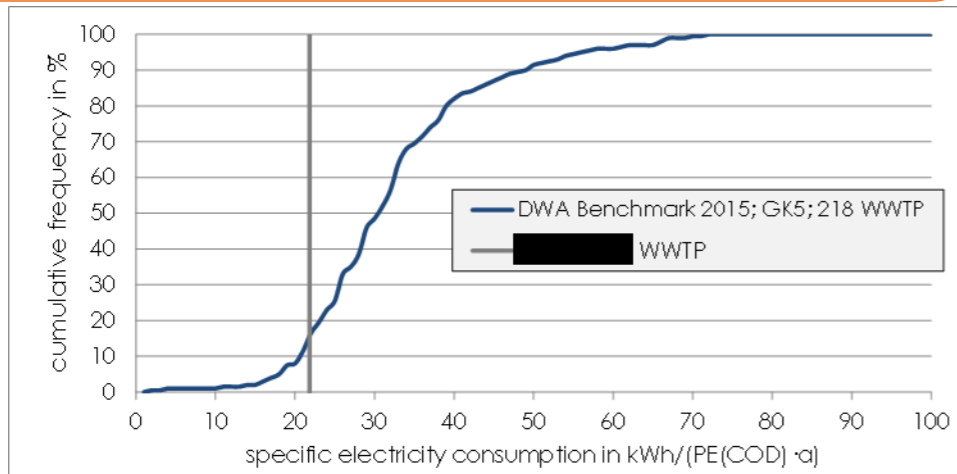




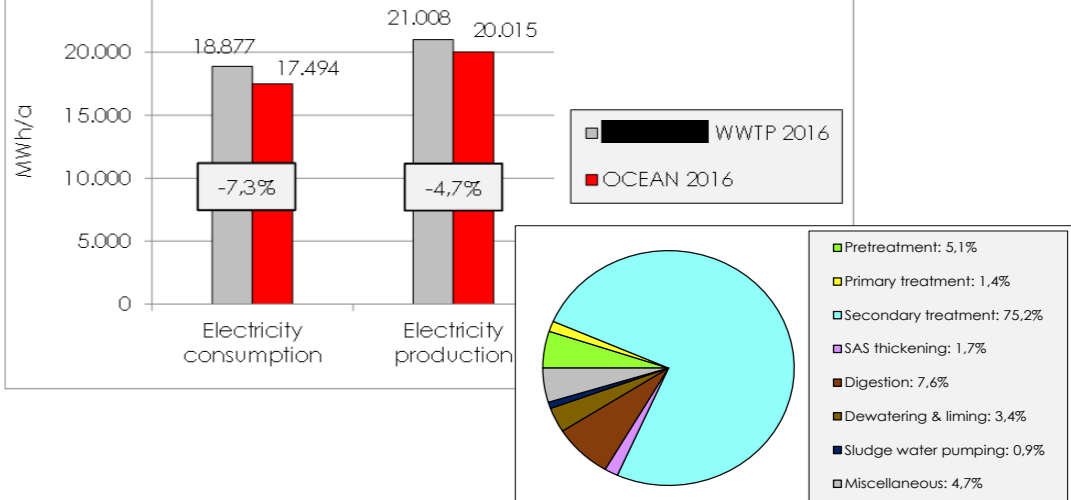
Audit deliverables



KPI comparison with benchmarks



OCEAN calibration results



Cost-benefit analysis of state-of-the-art measures

Action GI-2. Chemical enhancement of the primary settling

Technical Issues

In order to improve the outlet quality (especially phosphorus), we recommend to dose coagulant at the inlet of the primary settling. This way, the phosphorus concentration of the outlet of the primary settling could be reduced so the phosphorus load coming from the by-passed settled water could be decreased. With this action, it is possible to reach at the outlet of the main line lower P concentrations than the discharge requirement. In the other hand, additional COD will be removed and the biogas production could increase. However, the implementation of the Action GI-1 should avoid lack of oxygen for denitrification. The additional coagulant dosing in the ASP will still remain the same as the current dose will considerably decrease.

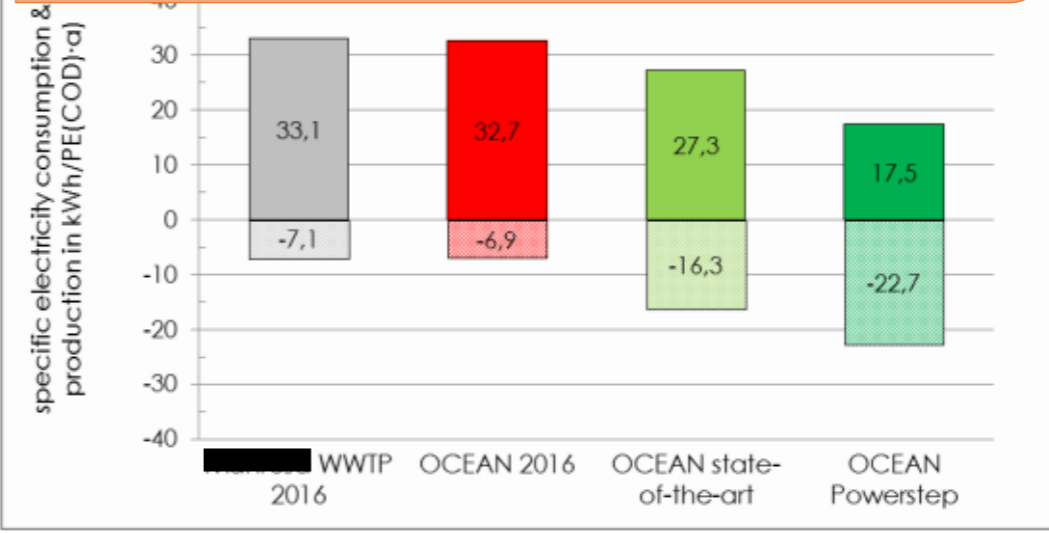
Key parameters and assumptions

- Assumed FeCl₃ dosing in the primary settling: 2.5 to 3 mg Fe/l
 - Additional coagulant consumption: 1,400 t/a → 176,000 €/a
- Calculated P outlet concentration: approx. 0.9 mg/l < 1 mg/l requirement
 - Liquid polymer savings for SAS mechanical thickening due to lower biological sludge production:
 - 20 t/a
 - 55,000 €/a liquid polymer savings
- Decrease of the purchased electricity due to the increase of electricity production: 1,940 MWh/a → 138,000 €/a
- Increase of sludge disposal: 1,330 t/a → 73,000 €/a

Cost Benefits Analysis

Investment costs	150,000 € for a coagulant storage and dosing station
Improvement outlet quality	0.9 mg/l P reached at the outlet
Costs savings	193,000 €/a (electricity & liquid polymer)
Additional costs	249,000 €/a (coagulant & sludge disposal)
Resulting additional costs	56,000 €/a

Savings potentials Powerstep scenario(s)





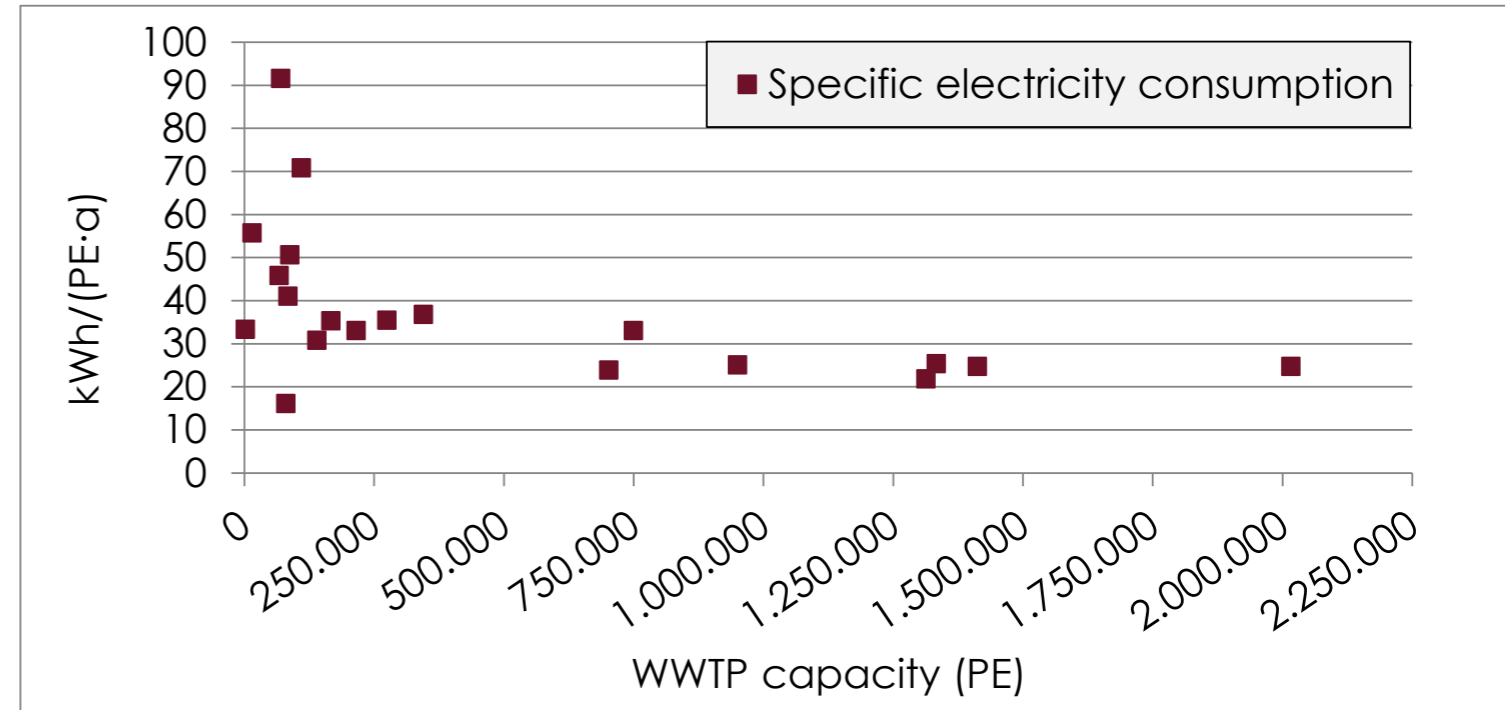
Current situation analysis – energy consumption



Electricity

Variance for plants < 100,000 PE

1. Staff skills
2. Outlet discharge requirements
3. Investment capacity



Heat

usually excess of heat production → no external consumption

Natural gas / fuel oil

Negligible except in special contexts:

- Sludge drying (w/o incineration)
- Oversized CHP





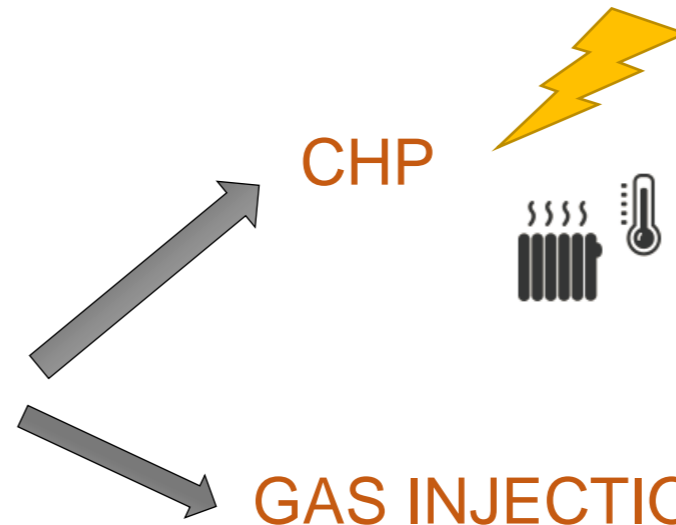
Current situation analysis – energy production



From digestion & biogas utilisation

15 WWTP

- Start from 60,000 / 170,000 PE
- depends on electricity & sludge disposal price levels



commonly used

Northern Europe

From sludge incineration

Heat export in 2 WWTP

Energy self-sufficiency is not a dream!

electricity self-sufficiency in 2 plants

Positive energy balance in another plant





Proposed state-of-the-art measures



Optimisation of control system

- *Aeration monitoring*
- *Recirculation rates*

...

Implementation of additional processes

- *Modification process configuration*
- *Digestion + biogas utilisation*

...

no
CAPEX



high
CAPEX

Optimisation of operating conditions

- *Decrease sludge age*
- *Decrease O₂ set point*
- *Optimise recirculation rates*
- *Optimise sludge water quality*

...

Equipment renewal

- *Aeration system (air diffusers + blowers or surface aerators)*
- *Mixing system of activated sludge tanks*
- *Pumps*

...





Proposed Powerstep concepts



WWTP < 50,000 PE

Chemically enhanced
microfiltration



Activated sludge process

WWTP > 50,000 PE

Chemical enhancement
of existing 1^{ary} settling

Chemically enhanced
microfiltration



Mainstream Anammox
1-stage IFAS process





Example with a 215,000 PE WWTP



- Underloaded (50% in average)
- not compliant for TN 11,7 > 10 mg/l requirement
- 33 kWh/(PE·a) electricity consumption > 65% of WWTP in DWA benchmark
- Only 20% electricity self-sufficiency

State-of-the-art measures:

1. *Optimisation of digestion temperature*
2. *Optimisation of SAS thickening*
3. *Optimisation of nitrogen removal*
4. *Implementation of more efficient air diffusers*
5. *Implementation of more efficient blowers*
6. *Implementation of more efficient CHP*

3. Implement aeration sequencing in nitrification tanks & increase MLSS recirculation rate

Cost Benefits Analysis	
Investment Cost	0 €
Improvement outlet quality	8,9 mg/l TN instead of 11,7 mg/l → compliance
Electricity additional consumption	154 MWh/a
Additional costs	16.900 €/a

2. Replace existing flotation by gravity belt thickening

Cost Benefits Analysis	
Investment Cost	150.000 €
Energy savings	413 MWh/a electricity
Polymer additional consumption	6,1 t/a
Sludge disposal savings	110 t/a
Consumable costs savings	32.600 €/a

5. Replace rotary lobe blowers by turbo & screw blowers

Cost Benefits Analysis	
Investment Cost	150.000 €
Electricity savings	185 MWh/a
Costs savings	20.400 €/a





Example with a 215,000 PE WWTP



Powerstep reduces electricity consumption...

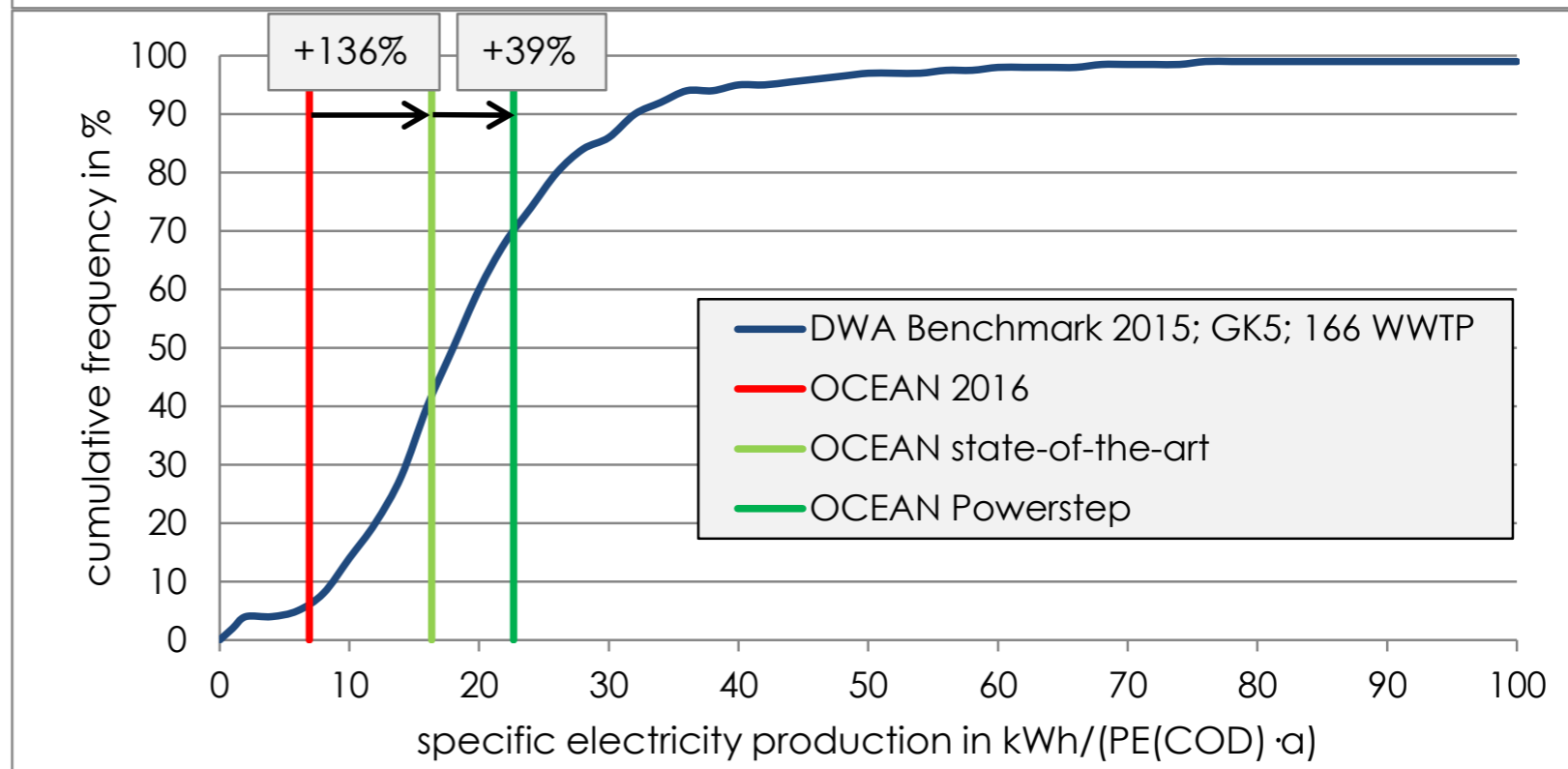
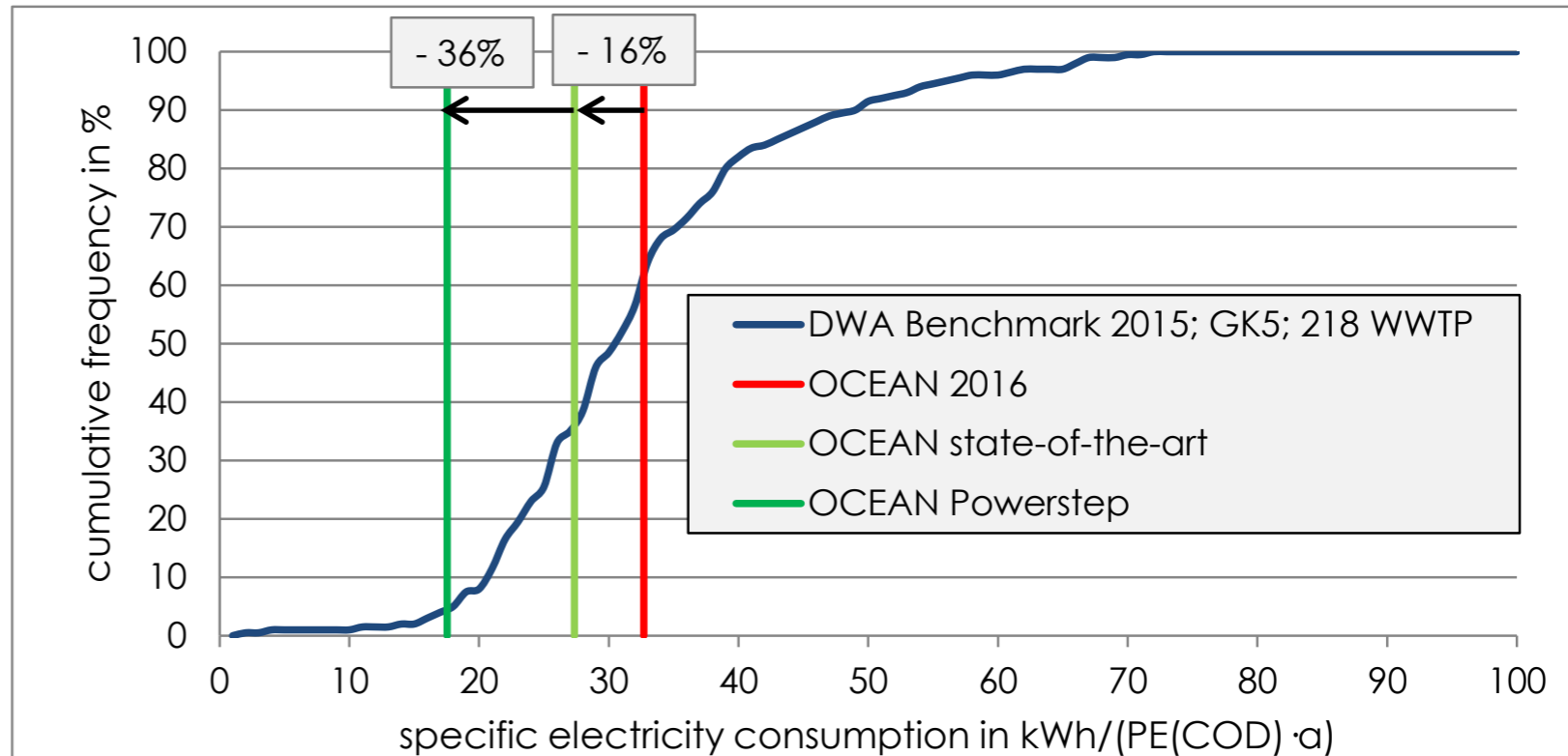
- Smaller volumes
- No MLSS recirculation
- Lower RAS rate

... and increases the production

- More sludge
- Higher methane potential

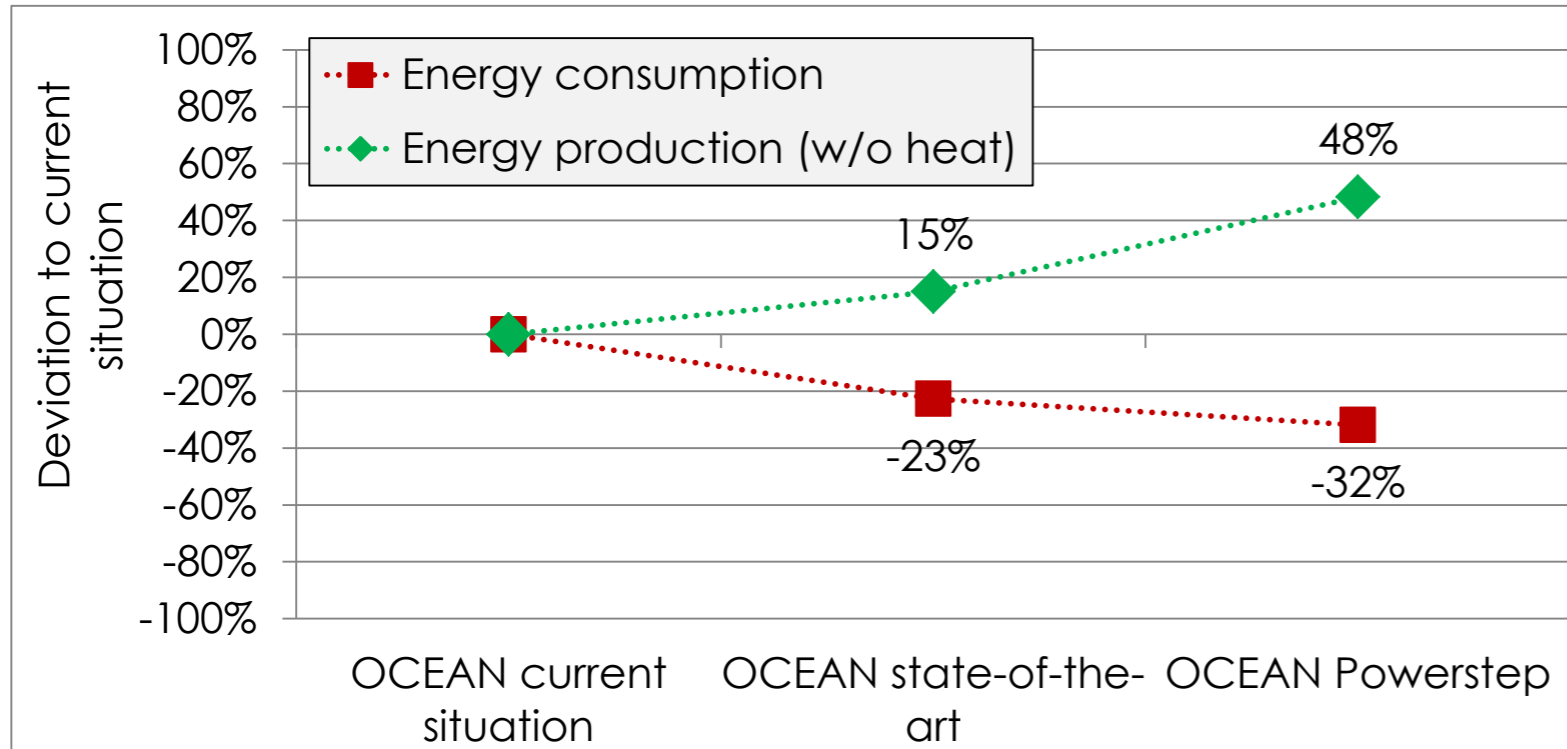
Potential to reach electricity self-sufficiency

1. Reach 60% through state-of-the-art measures
2. Reach 130% through Powerstep measures





Cumulative results so far*



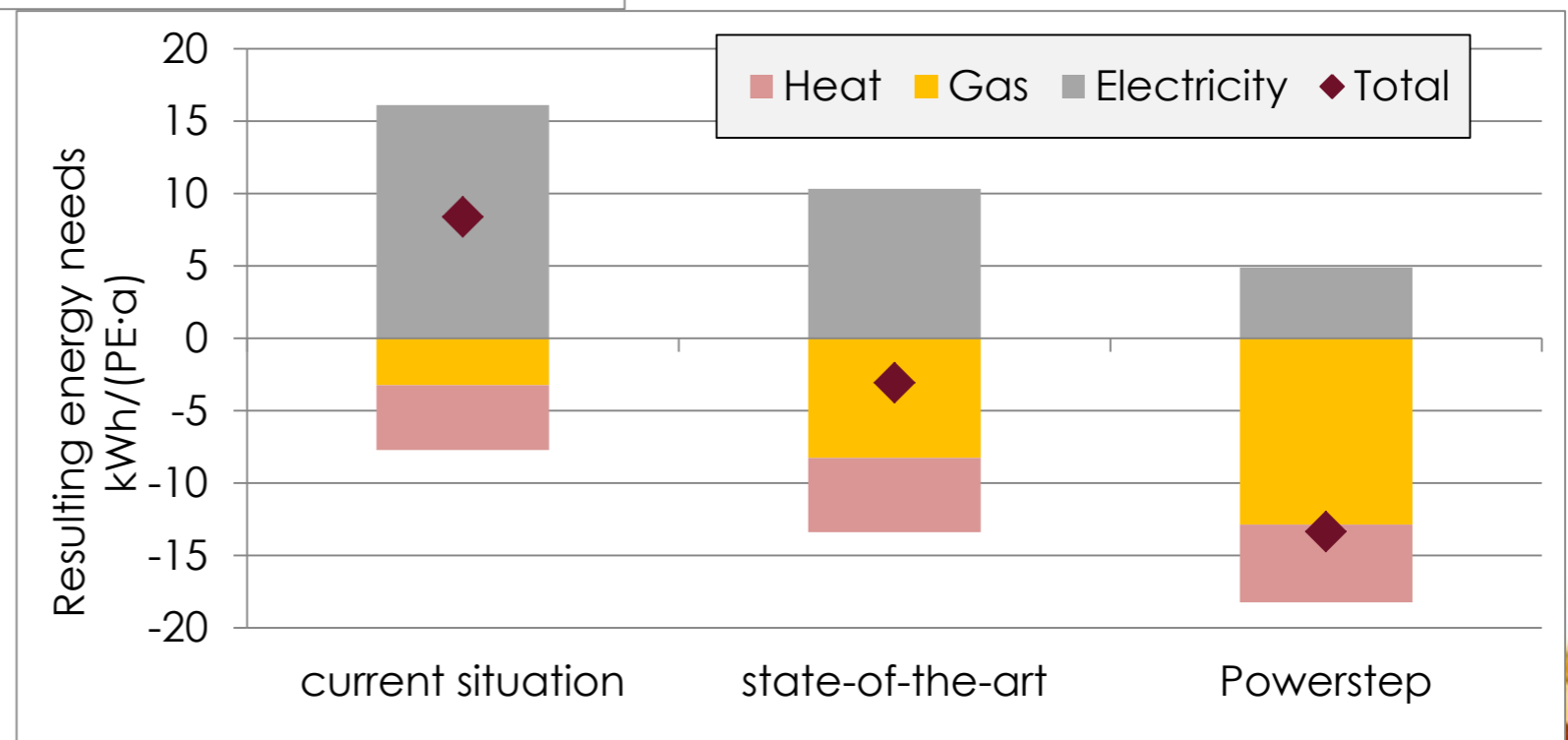
State-of-the-art measures:

- High energy savings
- Energy production at medium WWTP

Powerstep concepts:

- Limited energy savings...
- ... but high potential to increase energy production

Powerstep concepts lead to extend energy self-sufficiency to more WWTP (from 3 to 7 WWTP out of 11)



* Results based on 11 completed audits



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Take home messages



Energy self-sufficiency is a reality...
... but only in some plants with favourable conditions

First challenge should be to apply state-of-the-art technologies
& train operators in WWTP < 100,000 PE

Powerstep concepts significantly increase energy production
& enable new levels of energy-efficiency at WWTPs





Acknowledgement



POWERSTEP is an innovation action project supported by the European Union under the Horizon 2020 Framework Programme.

Contract no. 641661

Duration: 01/07/15 – 30/06/18





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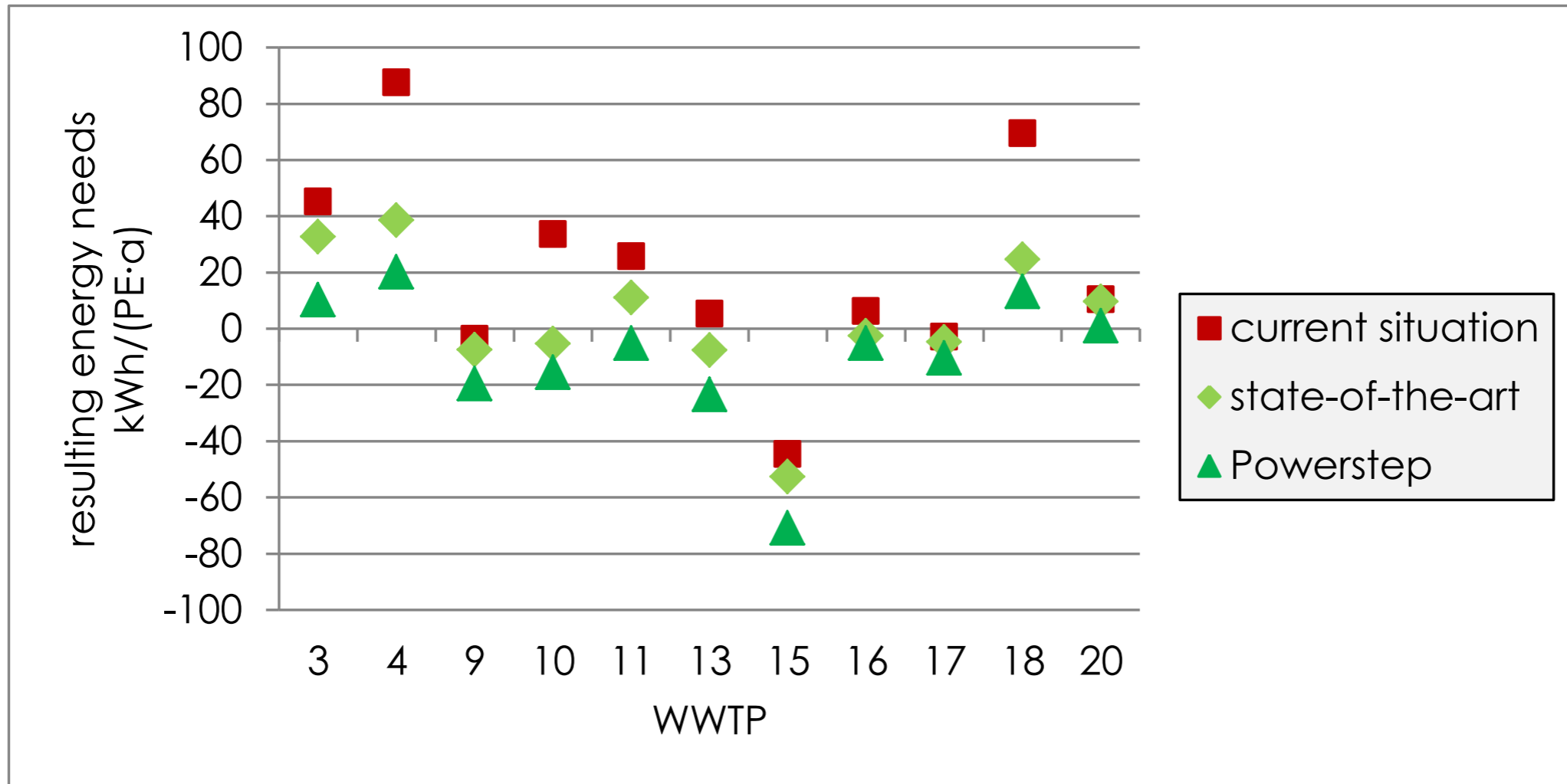


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Back-up slide – Energy balances



4 & 10: implementation of a digestion

15: heat and biogas selling

10, 13: biomethane selling

18: digestion but no utilised as it should be because biogas treatment is missing

